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INNOVATIVE SOLUTIONS FOR CORROSION CHALLENGES

Premature Failure of Radiant Shield Boiler Tubes in a Reformer Convection Section

A Failure Analysis Case Study



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CONTENT









INTRODUCTION

- In the reformer convection section, steam leakage from radiant shield boiler tubes was observed.
- The failure of the radiant shield boiler tubes resulted in a plant shutdown.
- The failure occurred ten days after start-up following a planned maintenance shutdown.
- During planned maintenance shutdown, UT thickness checks and visual examination did not revealed any issues in the boiler tubes.
- Failure analysis was conducted to identify the reason of tube failure.







BACKGROUND





• Boiler water from the steam drum flows inside the tubes from the inlet header (bottom).

• Heating on the external surface is through flue gas from the radiant section.

 The boiler has 4 rows of tubes with Row 1 being on the upstream side (US) and Row 4 being on the downstream side (relative to flue gas flow direction)

• The failures occurred on Row 1

• The material of construction is ASME SA 210 Gr C

VISUAL EXAMINATION



- Longitudinal cracking and bulging in multiple discolored areas along Row 1 tubes were observed
- The bulging and discoloration is typical of overheating damage
- Deposits inside the headers and tubes were observed •
- Heavy deposits can block tubes leading to overheating





VISUAL EXAMINATION

- 6 tubes were selected for analysis:
 - Row 1 5 tubes (tubes# 1, 5, 11, 47 & 78) with varying degrees of damage (opening, cracking, bulging, no apparent damage)
 - Row 4 1 tube with no apparent damage was selected for reference purposes
- The damage is on the upstream side (US) of the tubes (side facing the oncoming flue gas)
- Cracking is longitudinal and multiple
- Crack direction indicates that cracking is driven by stresses due to internal pressure (hoop stresses)
- Scaling and discoloration coinciding with the bulged and cracked areas is a sign of overheating











Longitudinal Cracking

VISUAL EXAMINATION



- The internal surfaces of the tubes were covered with loose whitish scale
- Internal scales can insulate the tube from the cooling effect of the water resulting in increased tube wall temperatures.
- One of the cracks was sectioned in the middle and cross sectional views revealed a thick walled fish mouth type of rupture which is typical of creep failures.









METALLOGRAPHY



Spheroidization occurs between 440°C and 760°C. May occur within few hours at 550°C but may take several years to
occur at 455°C (API 571).



- The creep threshold temperature for carbon steel is 371°C.
- Oxidation of carbon steel becomes significant above 450°C.
- All these temperatures are above the design temperature.

METALLOGRAPHY



- Banded structure Normal ; Equiaxed structure – recrystallization occurred •
- Transformation phase transformation occurred; Transformation occurs above 720°C.
- The microstructure indicates overheating.





Row 4, Tube 1 – Long. - US



METALLOGRAPHY

Row 1 ,Tube 5 – Long. – Bulge (US)



- Banded structure Normal ; Equiaxed structure recrystallization occurred •
- The microstructure indicates overheating.



Row 1, Tube 5 – Long. – Bulge (US)



-wall Mid

HARDNESS TEST





Row 4, Tube 1 – DS



Row 1, Tube 47 – Bulge



- in ASTM A370).
- phases upon cooling.
- due to spheroidization.



	ID	Middle	OD
US	129	142	131
DS	176	166	151
, Bulge	175	151	111
Crack	267	202	126

• The specified maximum hardness for ASME SA 210 Gr C tubes is 179HB (179HV according to the conversion table

• The hardness of tube 78 sample is higher than the specified maximum. This can be attributed to the transformation that resulted in formation of harder

• The specified minimum tensile strength for ASME SA 210 Gr C tubes is 415MPa (that's an equivalent hardness of 123HV according to the conversion table in ASTM A370).

• The hardness of tube 47 OD is below the approximate minimum hardness. This can be attributed to softening

CHEMICAL ANALYSIS / XRD

XRF: Tube Deposits		
Elements	Conc. wt%	
Ca	37.15	
0	36	
Р	13.72	
Fe	5.083	
С	4.15	
Mg	1.37	
Ni	0.386	
Cr	0.384	
Al	0.266	
Cu	0.2589	
S	0.231	
Мо	0.188	
Mn	0.173	
Si	0.0708	
Zn	0.0421	
Pb	0.0262	
Sr	0.0159	
Ti	0.012	

XRF: Header Deposits		
Elements	Conc. wt%	
0	35	
Ca	23.65	
Fe	11.71	
Мо	10.23	
Р	7.721	
Mg	5.73	
С	1.89	
Cu	0.7932	
Si	0.715	
Al	0.59	
Na	0.58	
Ni	0.5728	
Mn	0.124	
S	0.105	
Cr	0.091	
Zn	0.0882	
Sr	0.0289	
Cl	0.0212	
Ti	0.019	

Compound Name Powellite, syn Magnesium Iron O Hematite, syn Calcium Phosphate Oxide

- Compound Name Hematite, syn Calcium Phosphat Oxide Calcium Iron Oxide Siderite
- mainly from the water.
- been deposited in the boiler



XRD: Tube Deposits

	Formula	Semi Quant. (%)
	CaMoO ₄	33
xide	MgFe ₂ O ₄	16
	Fe ₂ O ₃	16
e	Ca ₁₀ (PO ₄) ₆ O	35

XRD: Header Deposits

	Formula	Semi Quant. (%)
	Fe ₂ O ₃	79
e	Ca ₁₀ (PO ₄) ₆ O	12
е	Ca ₂ Fe ₂ O ₅	2
	Fe(CO ₃)	7

• Chemical composition of the deposits indicates that they are

• Corrosion products from upstream equipment could have also

CONCLUSION

- Visual and metallographic examinations indicate that the cracking mechanism is creep.
- Visual, metallography and hardness testing indicate that the tubes were overheated.
- The overheating of the tubes was due to the presence of calcium-magnesium rich heavy deposits within the tubes.
- Deposits found inside the tubes restricted heat transfer between the flue gas and the water within the tubes, resulting in overheating, leading to the softening of the tube material and stress rupture due to creep.
- The nature of the deposits found inside the tubes are mostly originated from the boiler water system and indicate poor boiler feedwater treatment and monitoring.







THANK YOU

Reach out.





